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# Applied Catalysis B: Environmental

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# Surface Ba species effective for photoassisted $NO_x$ storage over Ba-modified $TiO_2$ photocatalysts



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#### ARTICLE INFO

Article history: Received 19 May 2015 Received in revised form 15 June 2015 Accepted 17 June 2015 Available online 23 June 2015

Keywords: Photocatalyst Nitrogen oxides NO<sub>x</sub> Titanium dioxide NO<sub>x</sub> storage

#### ABSTRACT

Surface modification of a  $TiO_2$  photocatalyst with Ba species was investigated in photoassisted nitrogen oxide ( $NO_x$ ) storage under UV-light irradiation. The  $NO_x$  storage capacity in the Ba-modified  $TiO_2$  photocatalyst was 1.4 times higher than that of the non-modified  $TiO_2$  photocatalyst. Structure and role of the surface Ba species on a  $TiO_2$  surface were characterized using temperature programmed reaction (TPR), diffuse reflectance infrared Fourier transform (DRIFT) spectroscopy, X-ray diffraction (XRD), X-ray photoemission spectroscopy (XPS), and transmission electron microscopy (TEM). The characterization results suggested that Ba-Ti mixed oxides with a two-dimensional layer and amorphous structure on a  $TiO_2$  surface were generated via decomposition of  $Ba(NO_3)_2$  precursors by  $O_2$  pretreatment at 773 K. Based on the results of the characterizations and the reactions, the generated Ba-Ti mixed oxides on a  $TiO_2$  surface stored  $NO_x$  more densely than the  $TiO_2$  surface; therefore, the generation improved the activity in the photoassisted  $NO_x$  storage under UV-light irradiation.

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# 1. Introduction

Control of nitrogen oxide  $(NO_x)$  emission in exhaust gas from engines is strongly required in terms of air purification. Many researchers and engineers have been challenged to develop efficient de- $NO_x$  technologies [1]. At the stoichiometric air-to-fuel (A/F) ratio of 14.7, three way catalysts are used for the  $NO_x$  removal [2,3]. However, under lean conditions (air-rich, A/F ratio: 20–65), typical three way catalysts cannot efficiently decompose the  $NO_x$  to harmless  $N_2$  although the lean operation of the engines leads to fuel economy and decreases of  $CO_2$  emission [4,5]. Two technologies have been developed for the removal of  $NO_x$  under the lean condition: selective catalytic reduction (SCR) and  $NO_x$  storage and reduction (NSR). In the SCR,  $NH_3$ , which is produced by decomposition of urea is introduced into the exhaust gas, and the introduced  $NH_3$  reduces the  $NO_x$  to  $N_2$ . The SCR have been investigated by many

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researchers since 1970s.  $V_2O_5$ -based catalysts [6–8] and Fe- or Cuzeolite catalysts [9] show high activity over 473 K. This technology is widely used in stationary emission sources and mobile emission sources including diesel engines in vehicles and trucks. However, the  $NO_x$  removal efficiency is low below 473 K.

Low-temperature removal of  $NO_x$  is highly desired in exhaust gas from vehicle engines. Regulation of  $NO_x$  emission has become severe year by year [10], and a recent report by the International Council for Clean Transportation (ICCT) pointed out the impact of the  $NO_x$  emission in the initial stage of engine start-up on the total emission amounts; in the cold start condition below 473 K (approximately  $800 \, \text{s}$ ), urea cannot be injected because of the low activity of the catalyst to avoid ammonia slip [11]. Thus, development of low temperature technology for  $NO_x$  removal is urgent task to improve the total removal efficiency of  $NO_x$  in the cold start condition.

On the other hand, the NSR technology was firstly reported by Toyota researchers in 1995 [5,12]. The NSR catalyst is composed of three components: precious metals, alkali or alkali earth oxides, and supports (e.g.,  $Pt/BaO/Al_2O_3$ ) [4]. In the lean condition, NO is oxidized on Pt sites and stored as nitrite ( $NO_2$ ) or nitrate ( $NO_3^-$ ) species. At that time, BaO functions as a  $NO_x$  storage material. After the  $NO_x$  storage in the lean condition, the engine is switched to the fuel-rich condition for a short time by injecting the fuels, and the

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stored  $NO_x^-$  is reduced by the injected fuels into  $N_2$  over Pt sites [4]. The lean and rich cycle operation provides the high  $NO_x$  removal efficiency [13]. However, the NSR catalysts also cannot reduce the  $NO_x$  efficiently at low temperatures below 473 K [14].

Photocatalysts are promising materials in terms of such a low temperature operation. Until now, several photocatalysts have been reported in the NO oxidation: TiO<sub>2</sub> [15], N-doped TiO<sub>2</sub> [16], metal-modified TiO<sub>2</sub> [17,18], TiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> binary oxide [19,20]. The reaction mechanism of NO oxidation was also investigated over the TiO<sub>2</sub> photocatalysts [21–28]. Recently, we demonstrated the Ba-modified TiO<sub>2</sub> photocatalysts showed high activity at a practical condition (gas hourly space velocity:  $50,000 \, h^{-1}$ , NO concentration: 200 ppm) under UV-light irradiation, and Ba modification of TiO<sub>2</sub> greatly enhanced the activity of NO<sub>x</sub> storage at low temperature [29]. The activity was improved after the pretreatment in  $O_2/He$ gas over 673 K, and the temperature corresponded to the decomposition temperature of  $Ba(NO_3)_2$  used as a Ba precursor. Thus, the activated Ba oxide species were generated during the pretreatment. The structure and the role of Ba oxide species are still unclear as the case now stands.

In Pt/BaO/Al<sub>2</sub>O<sub>3</sub> system of a typical NSR catalyst, classically, BaO and BaCO<sub>3</sub> species were assumed to be NO<sub>x</sub> storage materials [4,13]. On the other hand, BaO and Al<sub>2</sub>O<sub>3</sub> react at high temperature (>1073 K) to form an aluminate phase, BaAl<sub>2</sub>O<sub>4</sub> [30-32]. It was previously reported that the BaAl<sub>2</sub>O<sub>4</sub> was a better NO<sub>x</sub> storage material than BaO and/or BaCO<sub>3</sub> [30,31], although other groups reported that the generation of BaAl<sub>2</sub>O<sub>4</sub> decreased the performance [33]. In addition, TiO<sub>2</sub> was added to the NSR catalyst to improve the dispersion of Ba species using a strong interaction between Ba and Ti atoms [34], and the tolerance to sulfur poisoning [35–37], where the high temperature operations resulted in the generation of mix-oxide phase of Ti and Ba [34,38]. (e.g., BaTiO<sub>3</sub>) In our photocatalytic system, BaTiO<sub>3</sub> phase was observed after the pretreatment in  $O_2/He$  at 873 K, and the generation caused the decrease of  $NO_x$ storage activity [29]. Thus, the generation of mixed oxide phase and the effect on the activity should be considered to explain the role of Ba oxide species. In the present paper, the structure and role of Ba oxide species were investigated in the photoassisted NO<sub>x</sub> storage at low temperature to elucidate the Ba oxide species active for the  $NO_x$  storage.

#### 2. Experimental

# 2.1. Materials

 $TiO_2$  (ST-01, Ishihara Sangyo Kaisha, Ltd.) powder was used as purchased. Barium nitrate (Ba(NO<sub>3</sub>)<sub>2</sub>, 99.9%) and barium titanate (BaTiO<sub>3</sub>) were purchased from Wako Co., Ltd. (Japan).  $100-1000~\mu mol~g^{-1}~Ba/TiO_2$  catalysts were prepared by impregnation using a Ba(NO<sub>3</sub>)<sub>2</sub> precursor and a water (20 mL) as a solvent.

# 2.2. Activity tests

Photoassisted NO $_x$  storage was carried out using a fixed bed flow system. The detail was shown elsewhere [29]. Briefly, 0.13 g catalyst granules (diameter: 300–600  $\mu$ m) were added to a quarts reactor (12 mm  $\times$  10 mm  $\times$  1 mm, volume: 0.12 mL), and then pretreated at 773 K in 10% O $_2$ /He gas at 50 mL min $^{-1}$  for 1 h. The reaction gas (NO: 200 ppm, O $_2$ : 3%, He: balance) was flowed at 100 mL min $^{-1}$ . A 300 W Xe lamp (PerkinElmer PE300BF) was used as a light source. The NO $_x$  (NO+NO $_2$ ) in the outlet gas was analyzed using a portable gas analyzer (HORIBA PG-335). Dead time for NO $_x$  breakthrough, which was defined as a time when the outlet concentration of NO $_x$  reached to 2 ppm (conversion of NO: 99%), was used for NO $_x$  breakthrough in the present research.

#### 23 Characterization

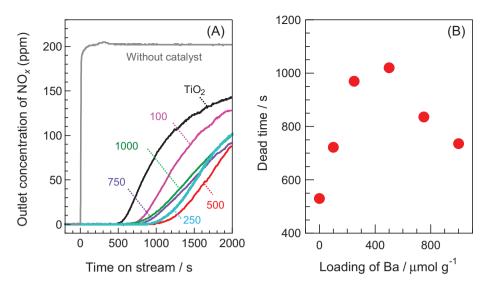
N<sub>2</sub> adsorption measurement was performed on a Belsorp-miniII (BEL, Japan) at 77 K. The specific surface area ( $S_{BET}$ ) was estimated from the N<sub>2</sub> adsorption isotherm using Brunauer-Emmett-Teller (BET) method. X-ray diffraction (XRD) measurement was carried out using a Rigaku Ultima IV X-ray diffractometer with Cu-Kα radiation ( $\lambda = 1.5406 \,\text{Å}$ ). The crystallite size was determined by the Scherrer equation using the full width at half maximum (FWHM) of the diffraction peak of anatase TiO<sub>2</sub> (101) plane. Temperatureprogrammed desorption (TPD) experiment was performed on the same experimental set-up as the activity test in 10% O<sub>2</sub>/He gas at 50 mL min<sup>-1</sup>. After the temperature was kept at 373 K for 30 min, the TPD measurement was started at a heating rate of 5 K min<sup>-1</sup> up to 973 K. The increase of temperature was also monitored using a thermocouple and an integrator. In situ diffuse reflectance infrared Fourier transform (DRIFT) spectra were measured using an ISDR-600 FTIR spectrometer (JASCO, Japan) equipped with a mercury-cadmium-tellurium (MCT) detector cooled by liquid nitrogen at a resolution of 4 cm<sup>-1</sup> with 16 co-added scans. The sample powder (50 mg) was placed in a diffuse reflectance cell, which was fitted by a potassium bromide (KBr) window at the top. The gas compositions of the pretreatment and the DRIFT experiment were the same as the activity tests. The catalyst was pretreated at 773 K, and then cooled to 373 K. A 200 W Hg-Xe lamp equipped with a collective lens (San-Ei Electric Co., Ltd., UVF-204S type C) was used as a light source. The background spectrum was measured after the pretreatment under a He gas flow at the 373 K. X-ray photoelectron spectroscopy (XPS) measurement was conducted on an ESCA-3400 spectrometer (Shimadzu, Japan). Sample was mounted on a silver sample holder by using a conductive carbon tape, and analyzed using Mg K $\alpha$  radiation in a vacuum chamber in 0.1 eV steps. The position of the carbon peak (284.6 eV) for C1s was used to calibrate the binding energy for all the samples. The surface atomic ratio was estimated from the band areas of XPS of Ba 3d, and Ti 2p, and the corresponding relative sensitivity factors [39]. Transmission electron microscopy (TEM) observation was carried out with JEOL-1400 TEM (JEOL, Japan).

#### 3. Results and discussion

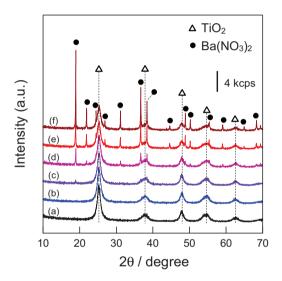
# 3.1. Effect of Ba loading

Fig. 1A represents the time course of  $NO_x$  storage over  $Ba/TiO_2$ catalysts with various Ba loadings. Without a catalyst, NO<sub>x</sub> concentration increased to 200 ppm immediately at the same time as NO/O<sub>2</sub> gas was introduced to the reactor. TiO<sub>2</sub> showed activity for NO<sub>x</sub> storage under UV-light irradiation, and the dead time for the  $NO_x$  breakthrough was 530 s. Loading of Ba drastically extended the dead time for NO<sub>x</sub> breakthrough for all the Ba loadings investigated as compared to TiO<sub>2</sub>. Fig. 1B shows the dead time in Fig. 1A as a function of Ba loading. The dead time increased with increasing the Ba loading up to  $500 \, \mu mol \, g^{-1}$ , and deceased over  $500 \, \mu mol \, g^{-1}$ . The dead time in  $500 \,\mu\text{mol}\,\text{g}^{-1}$  Ba/TiO<sub>2</sub> was  $1020 \,\text{s}$ , which was longer than the period during the cold start condition (800 s) reported by ICCT [11]. After the reaction after 12 h, the rates of  $NO_x$  storage were saturated, and the total amounts of stored NO<sub>x</sub> for 12 h of  $500 \,\mu\text{mol}\,\text{g}^{-1}\,\text{Ba/TiO}_2$  and  $\text{TiO}_2$  were  $560 \,\text{and}\,389 \,\mu\text{mol}\,\text{g}^{-1}$ , respectively. The modification of TiO<sub>2</sub> with Ba oxides species improved both the dead time and the total adsorption amount of  $NO_x$ .

The XRD patterns of  $TiO_2$  and as-synthesized Ba/ $TiO_2$  with various Ba loading showed diffraction peaks of anatase  $TiO_2$  (Fig. 2). Diffraction peaks of cubic Ba( $NO_3$ )<sub>2</sub> appeared in the as-synthesized Ba/ $TiO_2$  catalysts over 250  $\mu$ mol g<sup>-1</sup> of Ba loading, which indicates that the Ba species are loaded on  $TiO_2$  as a nitrate form after the



**Fig. 1.** (A) Time course of the photoassisted  $NO_x$  storage over  $Ba/TiO_2$  catalysts. Pretreatment temperature: 773 K, NO: 200 ppm,  $O_2$ : 2%, He: balance. The numbers represent Ba loadings ( $\mu$ mol  $g^{-1}$ ). (B) Effect of Ba loading on the dead time for the  $NO_x$  breakthrough.



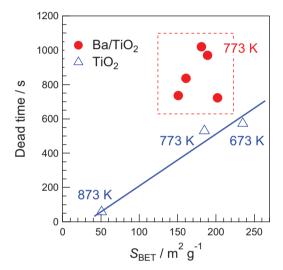
**Fig. 2.** XRD patterns of the as-synthesized Ba/TiO $_2$  catalysts with various Ba loading. (a) 0, (b) 100, (c) 250, (d) 500, (e) 750, and (f) 1000  $\mu$ mol g $^{-1}$ .

impregnation. Table 1 represents the crystalline size of  $TiO_2$  and  $S_{BET}$  of the catalysts with various Ba loading. In the as-synthesized catalysts,  $S_{BET}$  decreased with increasing the Ba loading although the crystalline size of  $TiO_2$  did not change after the Ba loading. The decrease of the surface area is possibly due to a plugging of

Table 1 Crystalline size of  ${\rm TiO_2}$  and BET specific surface area before and after the pretreatment and reaction.

Ba loading	da (nm)		$S_{BET}^{b} (m^2 g^{-1})$	
$(\mu molg^{-1})$	As-syn. <sup>c</sup>	ARd	As-syn.	AR
0	7.7	10.9	292	185
100	7.6	9.3	272	202
250	7.6	9.2	254	189
500	7.5	8.8	228	181
750	7.7	8.5	204	161
1000	7.7	8.5	181	151

- a Crystalline size of TiO2.
- b Specific surface area estimated from the BET method.
- <sup>c</sup> As-synthesized.
- <sup>d</sup> After the pretreatment at 773 K and the following NO<sub>x</sub> storage reaction.



**Fig. 3.** Correlation between  $S_{\text{BET}}$  and the dead time for the NO<sub>x</sub> breakthrough. Pretreatment temperatures were shown next to the symbols.

pores derived from gaps of TiO<sub>2</sub> particles [40]. Without Ba loading (bare TiO<sub>2</sub>), the pretreatment at 773 K and the following reaction drastically decreased S<sub>BET</sub> from 292 to 185 m<sup>2</sup> g<sup>-1</sup> and increased the crystalline sizes of TiO<sub>2</sub> from 7.7 to 10.9 nm, which was due to sintering of TiO<sub>2</sub> particles after the pretreatment at 773 K. The crystalline sizes of TiO<sub>2</sub> (8.5–9.3 nm) in Ba/TiO<sub>2</sub> after the reaction were smaller than that of TiO<sub>2</sub> after the reaction (10.9 nm). Thus, the Ba loading clearly suppressed the sintering of TiO<sub>2</sub> particles. To investigate of the effect of S<sub>BET</sub>, the dead time was plotted as a function of  $S_{\text{BET}}$  as shown in Fig. 3. The dead time increased with increasing S<sub>BET</sub> in the case of TiO<sub>2</sub> after the pretreatment at 673, 773, and 873 K (blue triangles). In the several photocatalytic reactions [21,41], the activity strongly depends on the surface area of the photocatalyst especially when the adsorption step of substrates is relatively slow. In this reaction, the strong positive correlation between the dead time and SBET was clearly observed, which suggests that the increase of  $S_{BET}$  would be effective to improve the activity. On the other hand, Ba/TiO2 photocatalyst (red circles) showed the significantly higher activity than those of  $TiO_2$  with similar  $S_{BET}$ . The activity improvement by the Ba loading cannot be explained by the surface area (i.e., sintering of TiO<sub>2</sub> particles). In addition, there was

no correlation between the dead time and  $S_{\rm BET}$  in Ba/TiO $_2$  with various Ba loading, which suggests that the dead time is dependent on the amount and state of Ba species. The total amount of stored NO $_X$  for 12 h of 500  $\mu$ mol g $^{-1}$  Ba/TiO $_2$  was 1.4 times higher than that of TiO $_2$  although  $S_{\rm BET}$  was almost the same as shown in Table 1. The results suggested that the Ba oxide species generated after the pretreatment at 773 K functioned as an effective NO $_X$  storage material.

#### 3.2. Correlation of the activity and TPD peak areas

TPD experiments were carried out using the as-synthesized Ba/TiO<sub>2</sub> catalysts to identify the active Ba precursors (Fig. 4A). Three desorption peaks were observed around 710, 800, and 850 K (referred to as peaks 1–3, respectively). The peak 1 was assigned to the decomposition of Ba(NO<sub>3</sub>)<sub>2</sub> in contact with a TiO<sub>2</sub> surface, and the peaks 2 and 3 were due to the decomposition of bulk Ba(NO<sub>3</sub>)<sub>2</sub> [29]. Two desorption peaks were observed in the TPD experiment using a Ba(NO<sub>3</sub>)<sub>2</sub> reference powder at 840 and 910 K, and the desorption temperatures were higher than those of Ba/TiO<sub>2</sub>. The low desorption temperatures in the Ba-modified catalysts were due to the interaction between TiO<sub>2</sub> and Ba species [38]. The peaks 2 and 3 were possibly due to the decomposition of the surface and inner part of bulk  $Ba(NO_3)_2$  [29]. The areas of peaks 1–3, which were estimated from a peak fitting using three Gaussians were plotted against the Ba loading (Fig. 4B). The area of peak 1 increased with the Ba loading up to  $500 \, \mu \text{mol} \, g^{-1}$ , and was saturated over  $500 \,\mu \text{mol}\,\text{g}^{-1}$ . On the other hands, the areas of peaks 2 and 3 showed the same tendency; the areas of two peaks were low below 250 µmol g<sup>-1</sup>, and the further increase of the Ba loading rapidly increased the areas of the two peaks. The same tendency supports the above assignment that peaks 2 and 3 were derived from the bulk  $Ba(NO_3)_2$ . As shown above, there are at least two  $Ba(NO_3)_2$  species in the as-synthesized Ba/TiO<sub>2</sub>; one is the surface Ba(NO<sub>3</sub>)<sub>2</sub> in contact with a TiO<sub>2</sub> surface, and the other one is the bulk Ba(NO<sub>3</sub>)<sub>2</sub> without a contact with a TiO<sub>2</sub> surface.

The effect of the Ba loading on the activity was explained by the amount of two Ba(NO<sub>3</sub>)<sub>2</sub> species estimated from the TPD spectra. The dead time in Fig. 1 increased with increasing the area of peak 1 derived from the surface Ba(NO<sub>3</sub>)<sub>2</sub>. The correspondence between activity and the amount of surface Ba(NO<sub>3</sub>)<sub>2</sub> indicated that the surface Ba(NO<sub>3</sub>)<sub>2</sub> on a TiO<sub>2</sub> is a precursor of active Ba oxide species for the  $NO_x$  storage. On the other hand, over  $500 \,\mu \text{mol g}^{-1}$ , the activity decreased in spite of the fact that the amount of the surface Ba(NO<sub>3</sub>)<sub>2</sub> (i.e., area of peak 1) did not change. The bulk  $Ba(NO_3)_2$ , which was inactive for the reaction [29] was generated, and the amount increased with the Ba loading. The increase of the Ba loading from 500 to  $1000 \, \mu mol \, g^{-1}$  decreased the  $TiO_2$  content in the catalyst by 13 wt% because the 500 and 1000  $\mu$ mol g<sup>-1</sup> corresponded to 13 and 26 wt%, respectively. The decrease of TiO<sub>2</sub> should decrease the activity because TiO2 works as an oxidation site in the reaction. Thus, amounts of the surface Ba(NO<sub>3</sub>)<sub>2</sub> and the inactive bulk Ba(NO<sub>3</sub>)<sub>2</sub> affected the activity, which resulted in the non-correlation between  $S_{\text{BET}}$  and the activity in Ba/TiO<sub>2</sub> in Fig. 3.

# 3.3. DRIFT investigation

DRIFT spectra were recorded at various exposure times of NO/O<sub>2</sub> gas in the dark. In the case of TiO<sub>2</sub> (Fig. 5A), the peaks at 1622, 1480, 1322, and 1194 cm<sup>-1</sup> increased with the exposure time of NO/O<sub>2</sub> gas. The peaks at 1480, 1322, and 1194 cm<sup>-1</sup> were assignable to NO<sub>2</sub><sup>-</sup> species, and the peak at 1622 cm<sup>-1</sup> to NO<sub>3</sub><sup>-</sup> species [42]. The co-adsorption of NO and O<sub>2</sub> produced NO<sub>2</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> species via adsorption and oxidation, which was in line with previous reports using several transition metals including TiO<sub>2</sub> [42–45]. After the irradiation, the peak intensity at 1194 cm<sup>-1</sup> monoton-

ically decreased with the irradiation time, which indicates that the  $NO_2^-$  species are consumed under irradiation. On the other hand, the intensities of new peaks at 1603, 1582, 1496, 1302, and 1249 cm<sup>-1</sup> increase and are saturated after 20 min of irradiation, which is due to the generation of  $NO_3^-$  species with bridging (1603, 1249 cm<sup>-1</sup>), chelating (1582, 1302 cm<sup>-1</sup>), and monodentate (1496 cm<sup>-1</sup>) forms [21,42,43]. Thus, the  $NO_2^-$  species are an intermediate in  $NO_x$  storage, and are oxidized into the  $NO_3^-$  species under irradiation (Eqs. (1) and (2)).

$$NO \xrightarrow{O_2, dark} NO_2^-, NO_3^-$$
 (1)

$$NO \xrightarrow{O_2,hv} NO_3^-$$
 (2)

DRIFT spectra in 500  $\mu$ mol g<sup>-1</sup> Ba/TiO<sub>2</sub> were shown in Fig. 5B. In the dark, peaks at 1620, 1477, 1379, and 1210 appeared after 30 min of an NO/O2 gas flow, and attribute to NO2- and NO3- species adsorbed on Ti sites because the peaks were observed in the case of TiO<sub>2</sub>. Other peaks were also observed at 1379 cm<sup>-1</sup> and around 1200 cm<sup>-1</sup> (shoulder peaks) in Ba/TiO<sub>2</sub>, which is possibly due to the NO<sub>2</sub><sup>-</sup> species [42]. Although a small difference was observed in the DRIFT spectra between TiO<sub>2</sub> and Ba/TiO<sub>2</sub> in the dark, the difference was not a direct evidence of the improvement of the activity by Ba loading under irradiation because the activity of NO<sub>x</sub> storage was quite low (no dead time) in the dark over Ba/TiO<sub>2</sub> [29]. The DRIFT spectra of Ba/TiO<sub>2</sub> after irradiation in NO/O<sub>2</sub> gas were similar to that in the case of TiO<sub>2</sub>; adsorption peaks at 1601, 1580, 1502, 1295, and 1254 cm<sup>-1</sup> increase with increasing the irradiation time for 3 h. The previous reports using BaO/Al<sub>2</sub>O<sub>3</sub> catalyst showed that NO<sub>2</sub> adsorbed on a BaO surface as ionic and bidentate NO<sub>3</sub>species and the adsorbed NO<sub>3</sub><sup>-</sup> shows the IR peaks at 1550 cm<sup>-1</sup> (bidentate), and 1320 and 1410 cm<sup>-1</sup> (ionic) [34,45]. In our DRIFT investigations, the bands were not observed under irradiation. The results clearly indicates that the bulk BaO is not generated on a TiO2 surface after the pretreatment. Absence of bulk BaO species suggests that Ba species are strongly interacted with TiO2 as reported previously [38].

# 3.4. XRD pattern and TEM image

Fig. 6 shows the XRD patterns of  $TiO_2$  and  $500 \, \mu mol \, g^{-1} \, Ba/TiO_2$ . In all the catalysts, the diffraction peaks of anatase  $TiO_2$  were observed. In as-synthesized  $Ba/TiO_2$ , the diffraction patterns of  $Ba(NO_3)_2$  was observed, and the pretreatment at  $773 \, K$  deceased the peak intensities. The decrease of the peak intensities is due to the decomposition of  $Ba(NO_3)_2$  on a  $TiO_2$  surface based on the TPD results. No other peak was observed after the pretreatment at  $773 \, K$ , which suggests the Ba oxide species had an amorphous structure. After the  $NO_x$  storage, the peaks derived from  $Ba(NO_3)_2$  did not change compared to  $Ba/TiO_2$  after the pretreatment. From TEM images (Fig. 7), the particle size of  $TiO_2$  in the as-synthesized  $Ba/TiO_2$  was approximately  $7-9 \, nm$ , which accorded to the crystalline size estimated from XRD (Table 1). The particle size hardly changed after the pretreatment at  $773 \, K$ , and the following reaction.

# 3.5. XPS measurement

Fig. 8A shows Ba  $3d_{5/2}$  XPS of the Ba-modified catalysts. The peak position of Ba  $3d_{5/2}$  XPS of the as-synthesized Ba/TiO<sub>2</sub> was 779.9 eV. The peak positions in Ba/TiO<sub>2</sub> after the pretreatment and the following reaction were 780.2 and 780.1 eV, respectively, and peak shift was hardly observed. The positions in the Ba-modified catalysts were different from that in the BaTiO<sub>3</sub> reference sample (778.8 eV). In all the Ba-modified catalysts, the peak positions of Ti  $2p_{3/2}$  were 458.4-458.5 eV (Fig. 8B), which were equal to that in TiO<sub>2</sub> (458.4 eV). In the case of BaTiO<sub>3</sub>, the peak position was 458.1 eV and was higher by 0.3-0.4 eV compared to the Ba-modified

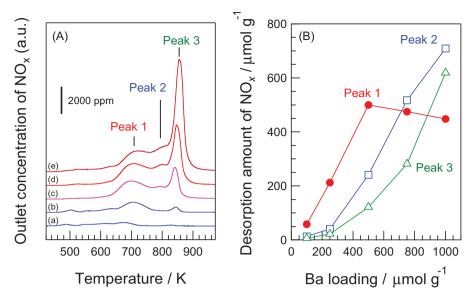


Fig. 4. (A) TPD profiles of as-synthesized Ba/TiO<sub>2</sub> catalyst with various Ba loadings of (a) 100, (b) 250, (c) 500, (d) 750, and (e) 1000  $\mu$ mol g<sup>-1</sup>. (B) Desorption amounts of NO<sub>x</sub> estimated from the peaks 1–3 as a function of Ba loading.

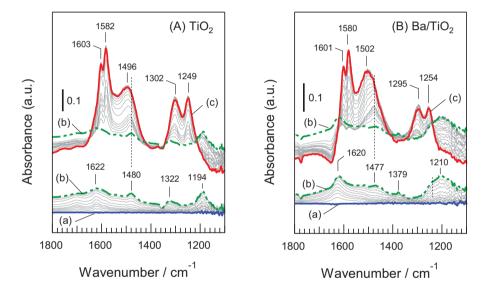


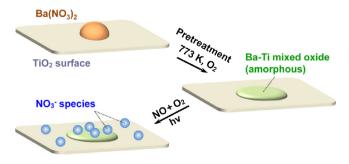
Fig. 5. DRIFT spectra of (A)  $TiO_2$  and (B)  $500 \mu mol g^{-1}$  Ba/ $TiO_2$ . After the pretreatment at 773 K: (a), after addition of  $NO/O_2$  gas for 30 min in the dark: (b), after irradiation for 3 h in  $NO/O_2$  gas: (c).

catalysts. The results indicate that the BaTiO<sub>3</sub> phase do not generated both after the pretreatment and the following reaction. The Ba/Ti surface atomic ratio was calculated from XPS. The pretreatment drastically increased the Ba/Ti ratio from 0.03 to 0.19, and decreased to 0.12 after the reaction. The increase in the Ba/Ti ratio clearly evidenced the structural change of Ba oxide species after the pretreatment, and can be explained by a two-dimensional layer structure of Ba oxide species. The two-dimensional structure of Ba species accorded with a model proposed by Emmez et al. using a substrate [46], and suggested the above-mentioned strong interaction between Ba oxide species and TiO<sub>2</sub>.

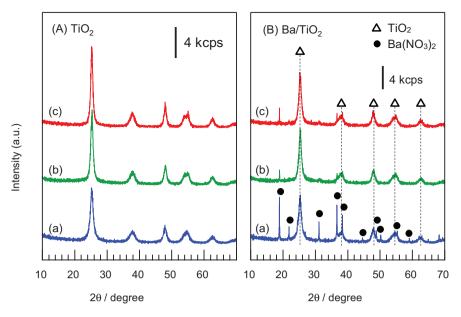
# 3.6. Active Ba species in photoassisted $NO_x$ storage

Surface model of the active Ba species for photoassisted  $NO_X$  storage is shown in Scheme 1. In as-synthesized catalysts,  $Ba(NO_3)_2$  precursors are loaded on a  $TiO_2$  surface. The  $O_2$  pretreatment at 773 K decomposes the surface  $Ba(NO_3)_2$  precursors to the active

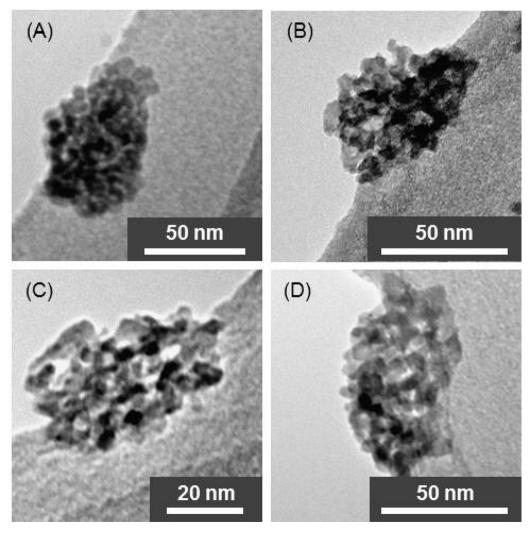
Ba species with an amorphous and two-dimensional layer structure with releasing  $NO_x$ . The DRIFT investigation revealed that the  $NO_3^-$  species were selectively adsorbed on Ti atoms after  $NO_x$  storage over Ba/TiO<sub>2</sub>, which indicates that the generated  $NO_3^-$  species did not directly adsorb onto Ba atoms. In our previous reports,



**Scheme 1.** Surface model of active Ba species for photoassisted  $NO_x$  storage.



 $\textbf{Fig. 6.} \ \ XRD \ patterns \ of (A) \ TiO_2 \ and (B) \ 500 \ \mu mol \ g^{-1} \ Ba/TiO_2. \ (a): as-synthesized, (b): after the pretreatment at 773 \ K, (c): after the reaction.$ 



 $\textbf{Fig. 7.} \ \ \text{TEM images of (A) TiO}_2, (B) \ \text{as-synthesized Ba/TiO}_2, (C) \ \text{Ba/TiO}_2 \ \text{after the pretreatment, and (D) Ba/TiO}_2 \ \text{after the reaction. Ba loading: } 500 \ \mu\text{mol g}^{-1}.$ 

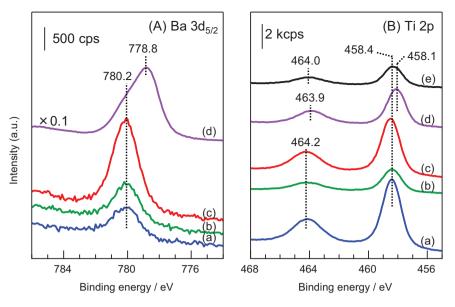


Fig. 8. XPS of (A) Ba  $3d_{5/2}$  and (B) Ti 2p, (a): as-synthesized, (b): after the pretreatment at 773 K, (c): after the reaction, (d): BaTiO<sub>3</sub>, (e): TiO<sub>2</sub>.

XRD pattern showed the generation of BaTiO<sub>3</sub> phase after the O<sub>2</sub> pretreatment at 873 K [29]. Although the BaTiO<sub>3</sub> phase was not observed after the pretreatment at 773 K from the XRD pattern in this report, TPR experiments clearly showed the decomposition of a part of Ba(NO<sub>3</sub>)<sub>2</sub> species after the pretreatment. Thus, the absence of bulk BaO species on a TiO<sub>2</sub> surface is possibly due to the generation of Ba-Ti mixed oxides on a TiO<sub>2</sub> surface with an amorphous structure. The generation of Ba-Ti mixed oxides coincide with the previous report by Emmez et al. [46]. They proposed the generation of perovskite-type Ba-Ti surface species (e.g., BaTiO<sub>3</sub>, and Ba<sub>2</sub>TiO<sub>4</sub>) with an amorphous structure after Ba deposition over TiO<sub>2</sub> films on a Pt(111) single crystal and following oxidation by  $O_2$  at 573–973 K using XPS and low energy electron diffraction (LEED). The selective adsorption of NO<sub>3</sub><sup>-</sup> onto Ti atoms observed in our DRIFT experiment using Ba/TiO<sub>2</sub> suggests that the NO<sub>3</sub><sup>-</sup> species were adsorbed on Ti sites on the Ba-Ti mixed oxides. Besides, the adsorption of NO<sub>x</sub> on perovskite compounds including BaTiO<sub>3</sub> was investigated previously, and these perovskites showed a high NO<sub>x</sub> storage capacity in spite of the low  $S_{BET}$ , (i.e., surface density of  $NO_x$  species was high on BaTiO<sub>3</sub>) [47]. In our experiments, 500 μmol g<sup>-1</sup> Ba/TiO<sub>2</sub> showed 1.4 times higher NO<sub>x</sub> storage capacity than the non-modified TiO<sub>2</sub> despite the similar  $S_{\text{BET}}$  values (Table 1). Thus, the amorphous Ba- $\overline{\text{Ti}}$ mixed oxides stored  $NO_3^-$  more densely than the  $TiO_2$  surface. We concluded that the Ba-Ti mixed oxides on a TiO2 surface function as an effective NO<sub>x</sub> storage material and the generation leads to the high activity in photoassisted NO<sub>x</sub> storage under UV-light irradiation.

#### 4. Conclusions

We demonstrated the surface modification of Ba species is an effective method to improve the activity in photoassisted  $\mathrm{NO}_x$  storage over  $\mathrm{TiO}_2$ -based photocatalysts under UV-light irradiation. The Ba loading affected the amounts of the surface and bulk  $\mathrm{Ba}(\mathrm{NO}_3)_2$  species in the as-synthesized catalysts, and the amounts predominated the activity. We proposed that the surface  $\mathrm{Ba}(\mathrm{NO}_3)_2$  was decomposed after the  $\mathrm{O}_2$  pretreatment at 773 K into the active Ba–Ti mixed oxides with an amorphous and two-dimensional layer structure. The surface Ba–Ti mixed oxides functioned as an effective  $\mathrm{NO}_x$  storage material, which leads to the high activity of the Ba-modified  $\mathrm{TiO}_2$  photocatalysts.

# Acknowledgments

This study was partially supported by the Program for Element Strategy Initiative for Catalysts & Batteries (ESICB), commissioned by the Ministry of Education, Culture, Sports, Science and Technology (MEXT) of Japan, and the Precursory Research for Embryonic Science and Technology (PRESTO), supported by the Japan Science and Technology Agency (JST). Akira Yamamoto thanks the JSPS Research Fellowships for Young Scientists.

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